

PERGAMON

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Letter to the Editors

Comments on "A fractal geometry model for evaluating permeabilities of porous preforms used in liquid composite molding"

In the recently published paper by Pitchumani and Ramakrishnan [1], the authors presented a fractal geometry model for evaluating permeabilities of porous preforms used in liquid composite molding. However, the model is highly questionable. Some comments are as the follows:

1. Eqs. (6)–(10) in the paper [1] lack the sound mathematical base.

According to Eqs. (2)–(5) in the paper [1], the definition of Q (page 2219): "total flow rate through the preform", and the further detailed definition of Q as (page 2223) "Further, the total volumetric flowrate, Q, through the representative preform volume is obtained by integrating the flowrate contribution by the pores in every $\mathrm{d}\lambda$ interval, over the entire range of prevalent pore sizes, λ_{\min} to λ_{\max} in the preform." The corresponding equations should be

$$Q = \int_{\lambda_{\min}}^{\lambda_{\max}} q(\lambda) \, dN(\lambda)$$

$$= g_q \frac{\Delta p}{\mu} \lambda_{\max}^3 \beta^{d_T} \left[d_N \frac{(1 - \alpha^{3 + d_T - d_N})}{3 + d_T - d_N} \right], \tag{C1}$$

$$k = \frac{\mu L_0 Q}{\Delta p A_0} = g_q \lambda_{\text{max}}^2 \beta^{1 + d_T} \left[d_N \frac{(1 - \alpha^{3 + d_T - d_N})}{3 + d_T - d_N} \right], \tag{C2}$$

$$\begin{split} v_p &= 1 - v_f = \frac{1}{L_0^2} \int_{\lambda_{\min}}^{\lambda_{\max}} g_v \lambda^2 \, \mathrm{d}N(\lambda) \\ &= g_v \beta^2 \left[d_N \left(\frac{1 - \alpha^{2 - d_N}}{2 - d_N} \right) \right], \end{split} \tag{C3}$$

$$\beta = \sqrt{\left(\frac{2 - d_N}{d_N}\right)},\tag{C4}$$

$$\alpha = \left(1 - \frac{1 - v_f}{g_v}\right)^{\frac{1}{2 - d_N}}.\tag{C5}$$

Eqs. (C1)–(C3) are the mathematically integrated results (see Appendix A for the detail). But this does not imply that Eqs. (C1)–(C3) are the correct fractal model for permeabilities. Eqs. (6)–(8) in the paper [1] can be obtained *only* by adding additional terms $g_q(\Delta P/\mu)\lambda_{\max}^3\beta^{d_T}$, $g_q\lambda_{\max}^2\beta^{d_T+1}$ and $g_v\beta^2$ into the right side of Eqs. (C1)–(C3),

respectively, and this means $Q + g_q(\Delta P/\mu)\lambda_{\max}^3 \beta^{d\tau} = Q$, $k + g_q \lambda_{\max}^2 \beta^{d_T+1} = k$ and $v_p + g_v \beta^2 = v_p$. From the definition of Q, Eqs. (C1)–(C3) should be the final results, therefore, there should be $Q + g_q(\Delta P/\mu)\lambda_{\max}^3 \beta^{d\tau} \neq Q$, so as to $k + g_q \lambda_{\max}^2 \beta^{d_T+1} \neq k$ and $v_p + g_v \beta^2 \neq v_p$, and thus Eqs. (6)–(8) are mathematically incorrect.

2. When the pore area fractal dimension $d_N=2$, $\beta=0$ from Eq. (9) and the model predicted permeability k=0 from Eq. (7), and Fig. 7 illustrates the results of the model. The paper [1] also states (page 2228) that "An interesting fact elucidated in Fig. 7(a) is that for any tortuosity dimension, as the area dimension, d_N , approaches its largest possible value of 2, the permeability approaches zero." However, when $d_N=2$, $\beta=0$ from Eq. (9) and $v_p=0$ (or $v_f=1$) from Eq. (8), this will result in $\alpha=1$ from Eq. (10). $\alpha=1$ corresponds to the physical situation of the preform consisting of pores with the size of $\lambda_{\min}=\lambda_{\max}$, and this will lead to the nonzero flowrate $(Q\neq 0)$ and non-zero permeability $(k\neq 0)$. Therefore, Eqs. (7)–(10) are contradictory each other.

As a result, the model proposed by Pitchumani and Ramakrishnan [1] is an erroneous one.

Eq. (3) (page 2222) in the paper [1] defines that "where d_N , the pore area dimension, is the fractal dimension of the intersecting pore cross-sections with a plane normal to the flow direction. Since d_N defines a fractal surface in a two-dimensional plane, its value lies in the range $1 < d_N < 2$." The paper [1] also states (page 2228) that "An interesting fact elucidated in Fig. 7(a) is that for any tortuosity dimension, as the area dimension, d_N , approaches its largest possible value of 2, the permeability approaches zero." Eqs. (6)–(8) DO yield the zero flow rate (Q = 0), zero permeability (k = 0) and zero pore volume fraction $(v_p = 0)$ as $d_N = 2$ (because $d_N = 2$, $\beta = 0$ from Eq. (9), Q = 0 from Eq. (6), k = 0 from Eq. (7) and $v_p = 0$ from Eq. (8)).

Actually, according to the definition on the "box counting method" (for evaluating the pore area dimension d_N given by the authors [1], page 2225), "N(L) now pertains to the number of boxes required to completely cover the pore areas." This will lead to $d_N = 2$ when a representative cross-section completely consists of pores or is only one pore, which means that the *pore* volume fraction v_p of this cross-section is 1. A cross-section with

 $v_p = 1$ will have the largest permeability for flow through this cross-section. Obviously, Eqs. (6)–(8) can be proved to be incorrect by themselves.

I here would like to give the following examples/references to further provide evidences.

Example 1: Skjeltorp [2], after using the "box counting method" for his experimental results, pointed out that (page 319) "It is also of interest to find D for different packing fractions (or coverage) defined as $\eta = packed$ area/total area. . . As expected, D approaches 2 as η increases toward 1 (compact structure with no holes)." In this paper [2], D is (page 320): "The fractal dimension of the packed regions." Compared with the paper [2], the pore in the paper [1] is corresponding to the packed in the paper [2]. Thus, the pore area fractal dimension d_N in the paper [1] will approach 2 as the *pore* volume fraction v_p (= pore area/total area) increases toward 1 (porous structure with no impermeable substance), and this $(v_p = 1)$ should result in the maximum permeability. This conclusion is exactly opposite to the model presented by Pitchumani and Ramakrishnan [1].

Example 2: Let us examine an another example, a generator of Sierpinski Carpet as shown in Fig. 1 (of the present paper), the pore area fractal dimension is $d_N = 1.8928$ [3] and the *pore* volume fraction is $v_p = 8/9$. If removing the central impermeable (black) substance from Fig. 1 (of the present paper), we have a square pore with the *pore* fractal dimension $d_N = 2$ and the *pore* volume fraction $v_p = 1$ as shown in Fig. 2 (of the present paper). It can be clearly seen that the permeability value of Fig. 2 (of the present paper) with $v_p = 1$ and $d_N = 2$ is higher than that of Fig. 1 (of the present paper) with $v_p = 8/9$ and $d_N = 1.8928$. In fact, the cross-section, as shown in Fig. 2 (of the present paper) with $v_p = 1$ and with $d_N = 2$, has the largest permeability compared with other Sierpinski Carpets with $v_p < 1$ and $d_N < 2$ in twodimensions.

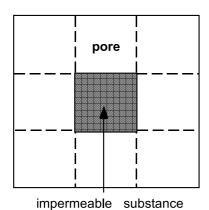


Fig. 1. A generator of Sierpinski Carpet with the pore fractal dimension $D_f = 1.8928$ and $v_p = 8/9$ and it has the lower permeability value than that of Fig. 2.

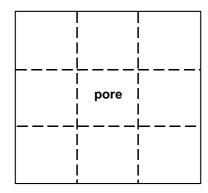


Fig. 2. A square pore with the pore fractal dimension $D_f = 2$ and $v_p = 1$ and it has the higher permeability value than that of Fig. 1

In addition to these two examples, some similar results and evidences can be found in many literatures [3–8].

Appendix A

From Eqs. (4) and (5) in the paper [1], the expression for Q is derived as (page 2223)

$$egin{aligned} Q &= -\int_{\lambda_{\min}}^{\lambda_{\max}} q(\lambda) \; \mathrm{d}N(\lambda) \ &= \int_{\lambda_{\min}}^{\lambda_{\max}} g_q rac{\Delta P}{L_c(\lambda)} rac{\lambda^4}{\mu} d_N rac{d\left(rac{\lambda}{\lambda_{\max}}
ight)}{\left(rac{\lambda}{\lambda_{\max}}
ight)^{d_N+1}} \ &= \int_{\lambda_{\min}}^{\lambda_{\max}} g_q rac{\Delta P}{L_c(\lambda)} rac{\lambda_{\max}^{d_N}}{\mu} d_N \lambda^{3-d_N} \; \mathrm{d}\lambda. \end{aligned}$$

With substitution of Eq. (2), we obtain

$$Q = \int_{\lambda_{\min}}^{\lambda_{\max}} g_q \frac{\Delta P}{L_0 \left(\frac{L_0}{\lambda}\right)^{d_T - 1}} \frac{\lambda_{\max}^{d_N}}{\mu} d_N \lambda^{3 - d_N} d\lambda$$

$$= g_q \frac{\Delta P}{\mu} \frac{\lambda_{\max}^{d_N}}{L_0^{d_T}} d_N \int_{\lambda}^{\lambda_{\max}} \lambda^{d_T - 1} \lambda^{3 - d_N} d\lambda.$$

Integrating and rearranging yields

$$Q = g_q \frac{\Delta P}{\mu} \frac{\lambda_{\max}^{d_T}}{L_0^{d_T}} \frac{\lambda_{\max}^{-(3+d_T-d_N)} \lambda_{\max}^3}{3+d_T-d_N} d_N (\lambda_{\max}^{3+d_T-d_N} - \lambda_{\min}^{3+d_T-d_N}).$$

According to the definition of $\beta = \lambda_{\text{max}}/L_0$ given in the paper [1], the expression evolves to

$$Q = g_q \frac{\Delta P}{\mu} \beta^{d_T} \frac{\lambda_{\max}^3}{3 + d_T - d_N} d_N \left(1 - \frac{\lambda_{\min}^{3 + d_T - d_N}}{\lambda_{\max}^{3 + d_T - d_N}} \right).$$

With the definition of $\alpha = \lambda_{min}/\lambda_{max}$ given in the paper [1].

$$Q = g_q \frac{\Delta P}{\mu} \lambda_{\text{max}}^3 \beta^{d_T} d_N \frac{(1 - \alpha^{3 + d_T - d_N})}{3 + d_T - d_N}.$$
 (A1)

Eq. (A1) can be rewritten as

$$Q = g_q \frac{\Delta P A_0}{\mu L_0} \frac{L_0}{A_0} \lambda_{\max}^3 \beta^{d_T} d_N \frac{(1 - \alpha^{3 + d_T - d_N})}{3 + d_T - d_N}.$$

Substituting $A_0 = L_0^2$ (page 2223) and $\beta = \lambda_{\text{max}}/L_0$ yields

$$Q = g_q \frac{\Delta P A_0}{\mu L_0} \lambda_{\max}^2 \beta^{d_T + 1} d_N \frac{(1 - \alpha^{3 + d_T - d_N})}{3 + d_T - d_N}.$$

Using Darcy's law, the permeability equation is derived as

$$k = \frac{\mu L_0 Q}{\Delta P A_0} = g_q \lambda_{\text{max}}^2 \beta^{d_T + 1} d_N \frac{(1 - \alpha^{3 + d_T - d_N})}{3 + d_T - d_N}.$$
 (A2)

The expression of porosity, Eq. (C3), can be obtained by the similar procedures. It can be seen that Eqs. (C1)–(C3) are the mathematically integrated results.

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